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U.S. Appl. No. 10/699,559 Response to Office Action dated April 7, 2005

IN THE CLAIMS

Please amend claims 1 - 9 and 11 - 16, cancel claim 10, and add new claims 17 - 22, as set forth below.

- 1. (currently amended) An integrated water treatment and flue gas desulfurization process comprising:
- (a) subjecting a water stream containing hardness minerals to a water treatment process using an alkali agent to precipitate the hardness minerals and raise the pH of the water stream to at least 8.5, to thereby producings a softened alkaline water stream having a pH of at least 8.5; and
- (b) utilizing the softened alkaline water stream <u>having a pH of at least 8.5</u> to scrub a flue gas containing sulfur dioxide to produce a sulfur-lean flue gas, wherein said flue gas containing sulfur dioxide is produced by burning a high-sulfur fuel.
- 2. (original) The process of claim 1 wherein the precipitating alkali agent is ammonia or aqueous ammonia.
- 3. (currently amended) The process of claim 1 wherein step (a) <u>comprises includes</u> the addition of the group consisting of sodium carbonate, carbon dioxide, sodium hydroxide, or magnesium oxide, <u>or and</u> any combination thereof.
- 4. (original) The process of claim 1 wherein the process is integrated with a steam injection bitumen recovery operation where step (b) further produces a treated water stream rich in sulfite/bisulfite for steam generation and underground steam injection and the water stream for step (a) is a produced water stream recovered from an underground reservoir.
- 5. (original) The process of claim 1 wherein step (a) includes a separation process to separate mineral precipitates from the softened water stream.

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- 6. (original) The process of claim 1 wherein the water stream for step (a) has a temperature of at least 85 degrees Celsius and not more than 100 degrees Celsius.
- 7. (original) The process of claim 1 wherein step (a) includes addition of carbon dioxide gas or sodium carbonate as a source of carbonate for precipitating calcium carbonate.
- 8. (currently amended) The process of claim 1-3 wherein the CO₂ can be a slipstream of the treated flue gas.
- 9. (original) The process of claim 1 wherein the alkali precipitating agent is a combination of excess ammonia and magnesium oxide.
- 10. (currently cancelled) The process of claim 1 wherein in step (a) the pH of the water stream is raised to at least 8.5.
- 11. (original) The process of claim 1 wherein in step (a) the pH of the water stream is raised to at least 9.3.
- 12. (original) The process of claim 4 wherein the treated water stream has a pH of at least 6.8 and not more than 7.2.
- 13. (currently amended) An integrated water treatment and flue gas desulfurization process comprising:
- (a) subjecting produced water containing hardness minerals and recovered from an underground reservoir in a steam injection bitumen recovery operation to a water treatment process using an alkali agent selected from the group consisting of ammonia, aqueous ammonia, and sodium hydroxide, and any combination thereof to precipitate the

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hardness minerals and raise the pH of the produced water to at least 8.5, to thereby producinge a softened alkaline water stream having a pH of at least 8.5; and,

- utilizing the softened alkaline water stream having a pH of at least 8.5 to (b) scrub a flue gas containing sulfur dioxide to produce a sulfur-lean flue gas and a treated water stream rich in sulfite/bisulfite for steam generation and underground steam injection, wherein said flue gas containing sulfur dioxide is produced by burning a high sulfur fuel.
- 14. (original) The process of claim 13 wherein step (a) includes a separation process to separate mineral precipitates from the softened water stream.
- 15. (original) The integrated water treatment and flue gas desulfurization process of claim 13 wherein step (a) includes the addition of magnesium oxide for silica removal.
- 16. (original) The process of claim 13 wherein step (a) includes the addition of carbon dioxide or sodium carbonate to enhance the precipitation of hardness minerals.
- The process of claim 1 wherein the high sulfur fuel is bitumen. 17. (new)
- The process of claim 1 wherein the high sulfur fuel is bitumen resid. 18. (new)
- The process of claim 1 wherein the high sulfur fuel is asphalt. 19. (new)
- The process of claim 13 wherein the high sulfur fuel is bitumen. 20. (new)
- The process of claim 13 wherein the high sulfur fuel is bitumen resid. 21. (new)
- The process of claim 13 wherein the high sulfur fuel is asphalt. 22. (new)